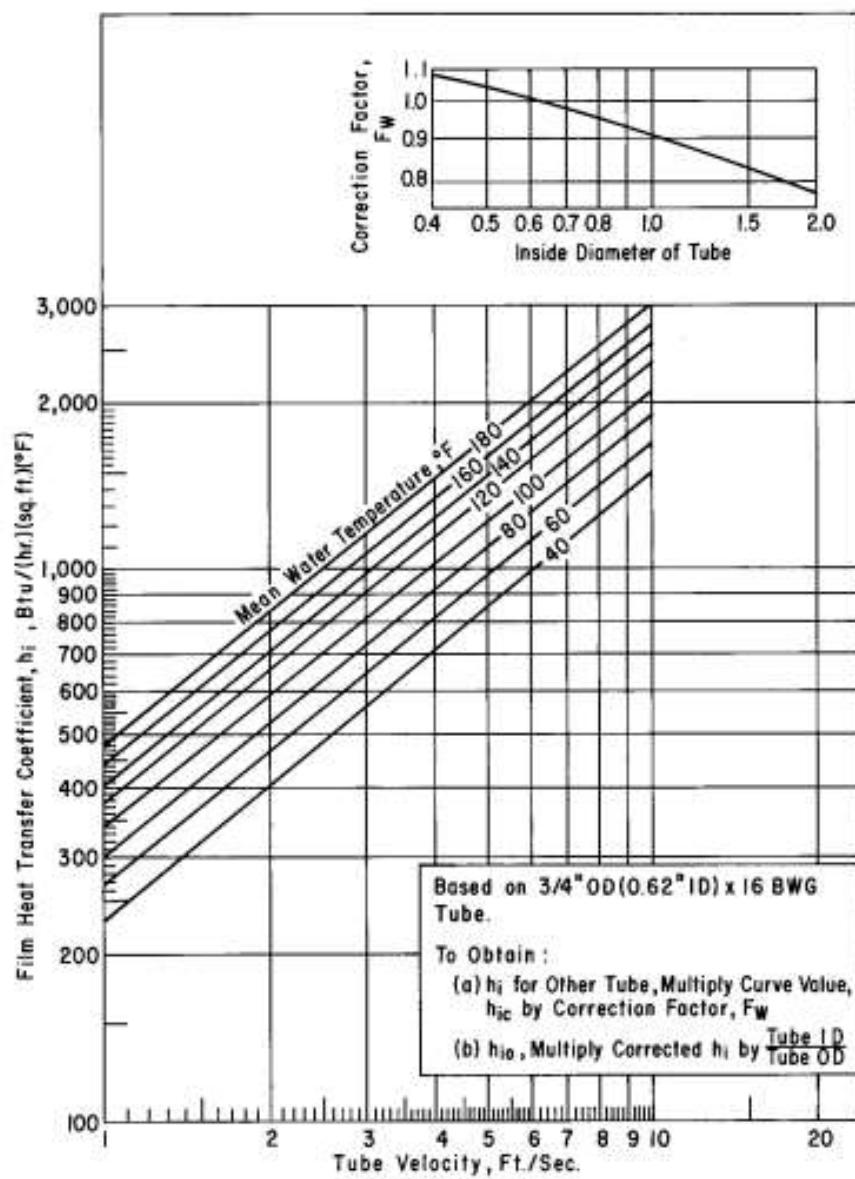




**Table 10-9**  
**Heat Exchanger Tubesheet Layout Tube Count Table**

Note the right column for tubesheet and number of passes per configuration.																
37	35	33	31	29	27	25	23 1/4	21 1/4	19 1/4	17 1/4	15 1/4	13 1/4	12	10	8	L.D. of Shell (in.)
1,269	1,143	1,019	881	763	663	553	481	391	307	247	193	135	105	69	33	3/4 in. on 15/16 in.Δ
1,127	1,007	889	765	667	577	493	423	343	277	217	157	117	91	57	33	3/4 in. on 1 in.Δ
965	865	765	665	587	495	419	355	287	235	183	139	101	85	53	33	3/4 in. on 1 in.□
699	633	551	481	427	361	307	247	205	163	133	103	73	57	33	15	1 in. on 1 1/4 in.Δ
595	545	477	413	359	303	255	215	179	139	111	83	65	45	33	17	1 in. on 1 1/4 in.□
1,242	1,088	964	846	734	626	528	452	370	300	228	166	124	94	58	32	3/4 in. on 15/16 in.Δ
1,088	972	858	746	646	556	468	398	326	264	208	154	110	90	56	28	3/4 in. on 1 in.Δ
946	840	746	644	560	486	408	346	280	222	172	126	94	78	48	26	3/4 in. on 1 in.□
688	608	530	462	410	346	292	244	204	162	126	92	62	52	32	16	1 in. on 1 1/4 in.Δ
584	524	460	402	348	298	248	218	172	136	106	76	56	40	26	12	1 in. on 1 1/4 in.□
1,126	1,008	882	768	648	558	460	398	304	234	180	134	94	64	34	8	3/4 in. on 15/16 in.Δ
1,000	882	772	674	566	484	406	336	270	212	158	108	72	60	26	8	3/4 in. on 1 in.Δ
884	778	688	586	506	436	362	304	242	188	142	100	72	52	30	12	3/4 in. on 1 in.□
610	532	466	396	340	284	234	192	154	120	84	58	42	26	8	XX	1 in. on 1 1/4 in.Δ
526	464	406	356	304	256	214	180	134	100	76	58	38	22	12	XX	1 in. on 1 1/4 in.□
1,072	1,024	904	788	680	576	484	412	332	266	196	154	108	84	48	XX	3/4 in. on 15/16 in.Δ
1,024	912	802	692	596	508	424	360	292	232	180	134	96	72	44	XX	3/4 in. on 1 in.Δ
880	778	688	590	510	440	366	308	242	192	142	126	88	72	48	XX	3/4 in. on 1 in.□
638	560	486	422	368	308	258	212	176	138	104	78	60	44	24	XX	1 in. on 1 1/4 in.Δ
534	476	414	360	310	260	214	188	142	110	84	74	48	40	24	XX	1 in. on 1 1/4 in.□
1,092	976	852	740	622	534	438	378	286	218	166	122	84	56	28	XX	3/4 in. on 15/16 in.Δ
968	852	744	648	542	462	386	318	254	198	146	98	64	52	20	XX	3/4 in. on 1 in.Δ
852	748	660	560	482	414	342	286	226	174	130	90	64	44	24	XX	3/4 in. on 1 in.□
584	508	444	376	322	266	218	178	142	110	74	50	36	20	XX	XX	1 in. on 1 1/4 in.Δ
500	440	384	336	286	238	198	166	122	90	66	50	32	16	XX	XX	1 in. on 1 1/4 in.□
1,106	964	844	732	632	532	440	372	294	230	174	116	80	XX	XX	XX	3/4 in. on 15/16 in.Δ
964	852	744	640	548	464	388	322	258	202	156	104	66	XX	XX	XX	3/4 in. on 1 in.Δ
818	724	634	536	460	394	324	266	212	158	116	78	54	XX	XX	XX	3/4 in. on 1 in.□
586	514	442	382	338	274	226	182	150	112	82	56	34	XX	XX	XX	1 in. on 1 1/4 in.Δ
484	430	368	318	268	226	184	154	116	88	66	44	XX	XX	XX	XX	1 in. on 1 1/4 in.□
1,058	944	826	716	596	510	416	358	272	206	156	110	74	XX	XX	XX	3/4 in. on 15/16 in.Δ
940	826	720	626	518	440	366	300	238	184	134	88	56	XX	XX	XX	3/4 in. on 1 in.Δ
820	718	632	534	458	392	322	268	210	160	118	80	56	XX	XX	XX	3/4 in. on 1 in.□
562	488	426	356	304	252	206	168	130	100	68	42	30	XX	XX	XX	1 in. on 1 1/4 in.Δ
478	420	362	316	268	224	182	152	110	80	60	42	XX	XX	XX	XX	1 in. on 1 1/4 in.□
1,040	902	790	682	576	484	398	332	258	198	140	94	XX	XX	XX	XX	3/4 in. on 15/16 in.Δ
902	798	694	588	496	422	344	286	224	170	124	82	XX	XX	XX	XX	3/4 in. on 1 in.Δ
760	662	576	490	414	352	286	228	174	132	94	XX	XX	XX	XX	XX	3/4 in. on 1 in.□
542	466	400	342	298	240	190	154	120	90	66	XX	XX	XX	XX	XX	1 in. on 1 1/4 in.Δ
438	388	334	280	230	192	150	128	94	74	XX	XX	XX	XX	XX	XX	1 in. on 1 1/4 in.□
1,032	916	796	688	578	490	398	342	254	190	142	102	68	XX	XX	XX	3/4 in. on 15/16 in.Δ
908	796	692	600	498	422	350	286	226	170	122	82	52	XX	XX	XX	3/4 in. on 1 in.Δ
792	692	608	512	438	374	306	254	194	146	106	70	48	XX	XX	XX	3/4 in. on 1 in.□
540	464	404	340	290	238	190	154	118	90	58	38	24	XX	XX	XX	1 in. on 1 1/4 in.Δ
456	396	344	300	254	206	170	142	98	70	50	34	XX	XX	XX	XX	1 in. on 1 1/4 in.□
37	35	33	31	29	27	25	23 1/4	21 1/4	19 1/4	17 1/4	15 1/4	13 1/4	12	10	8	L.D. of Shell (in.)



**Figure 10-50A.** Tube-side film heat transfer coefficient for water.  
(Used by permission: Kern, D. Q., *Process Heat Transfer*, 1<sup>st</sup> Ed., ©1950. McGraw-Hill, Inc. All rights reserved. Original adapted from Eagle and Ferguson, *Proc. Royal Society A* 127, 450, ©1930.)

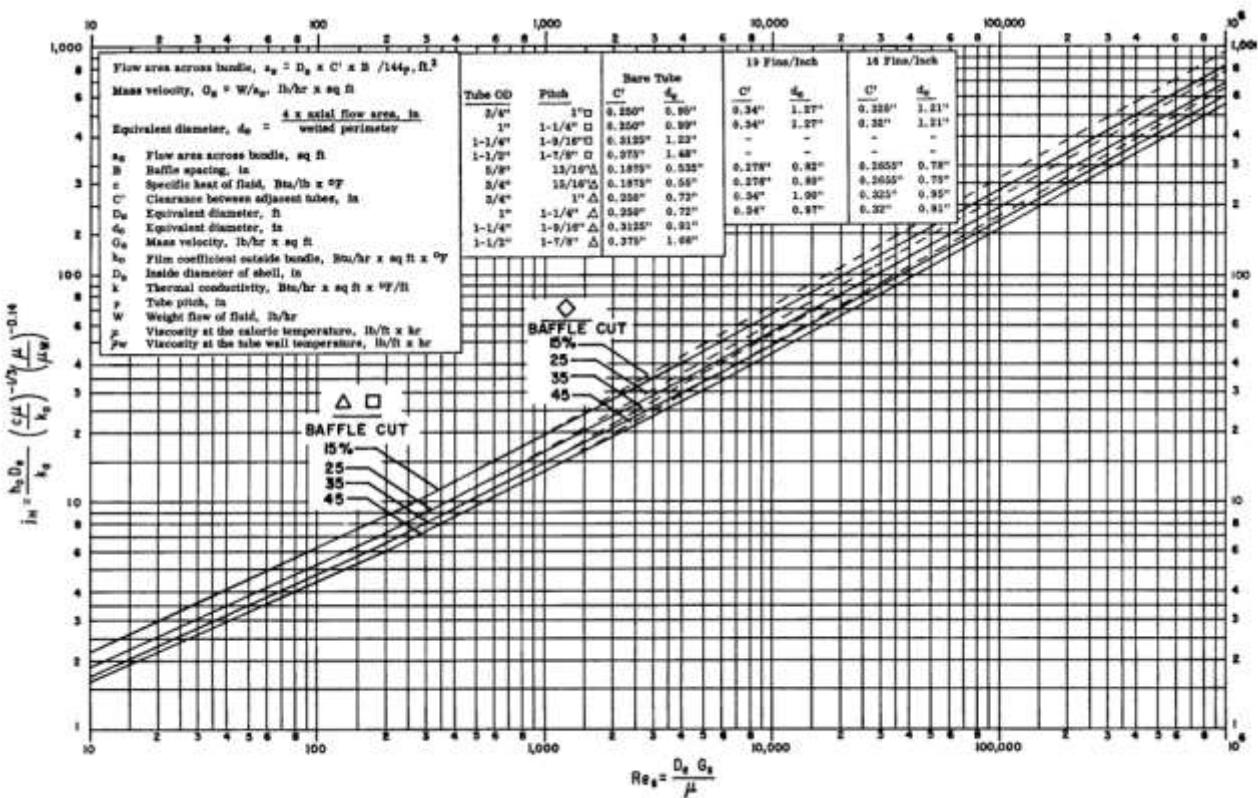
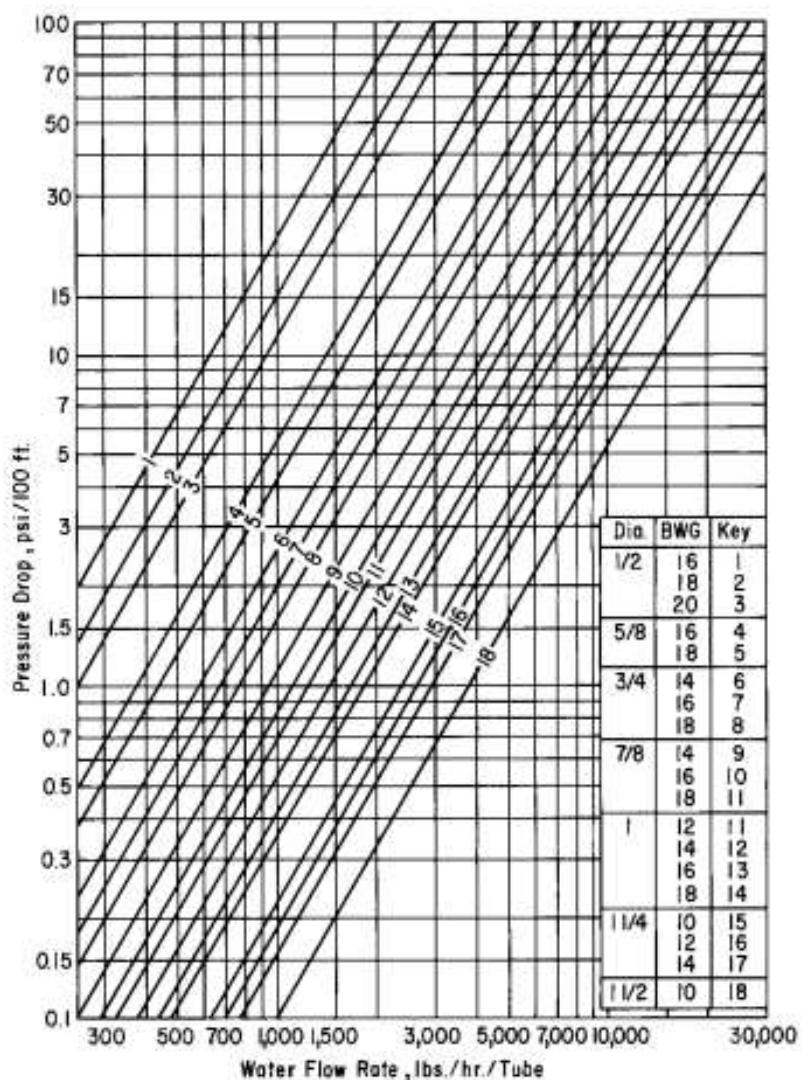


Figure 10-54. Shell-side heat transfer curve for segmental baffles. (Used by permission: Engineering Data Book Section II, ©1959, Wolverine Tube, Inc.)



(1) For Water Temperature of 120°F.,  $\Delta P_t$  Decreases about 6%.  
 For Most Applications Temperature Correction is not Significant.  
 (2) Increase  $\Delta P_t$  by 20% to Allow for Effect of Usual Fouling.

**Figure 10-138. Pressure drop for water in smooth tubes at 68°F.**  
 (Used by permission: *Scovill Heat Exchanger Tube Manual*, 3<sup>rd</sup> Ed.  
 Scovill Manufacturing Co.)

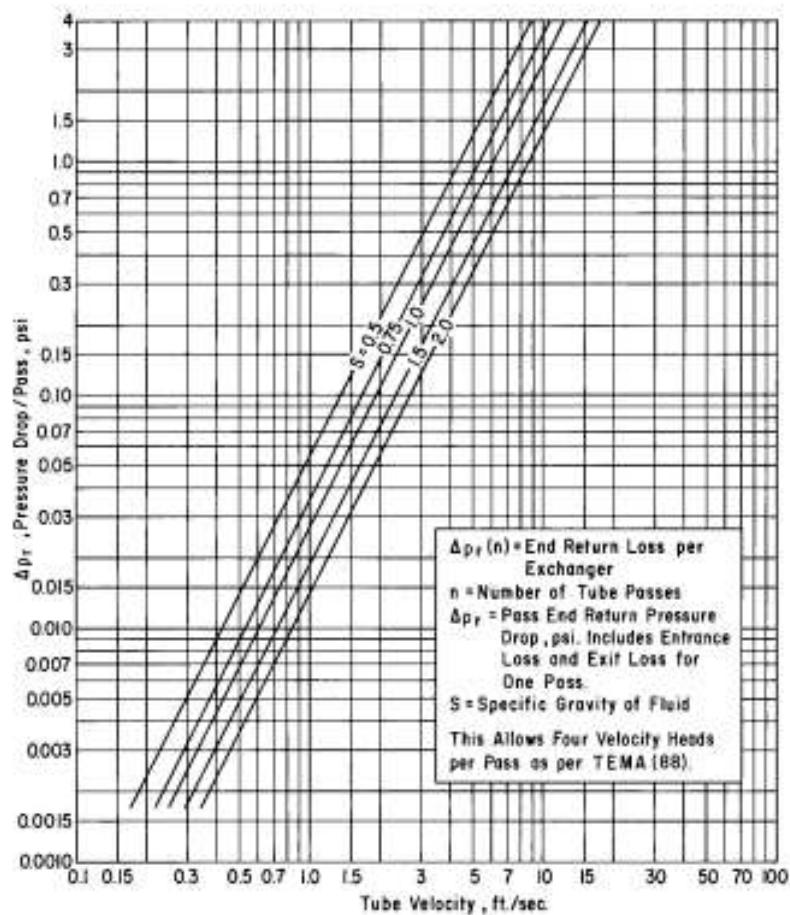


Figure 10-139. Tube side end return pressure drop per tube pass; viscosity close to water.

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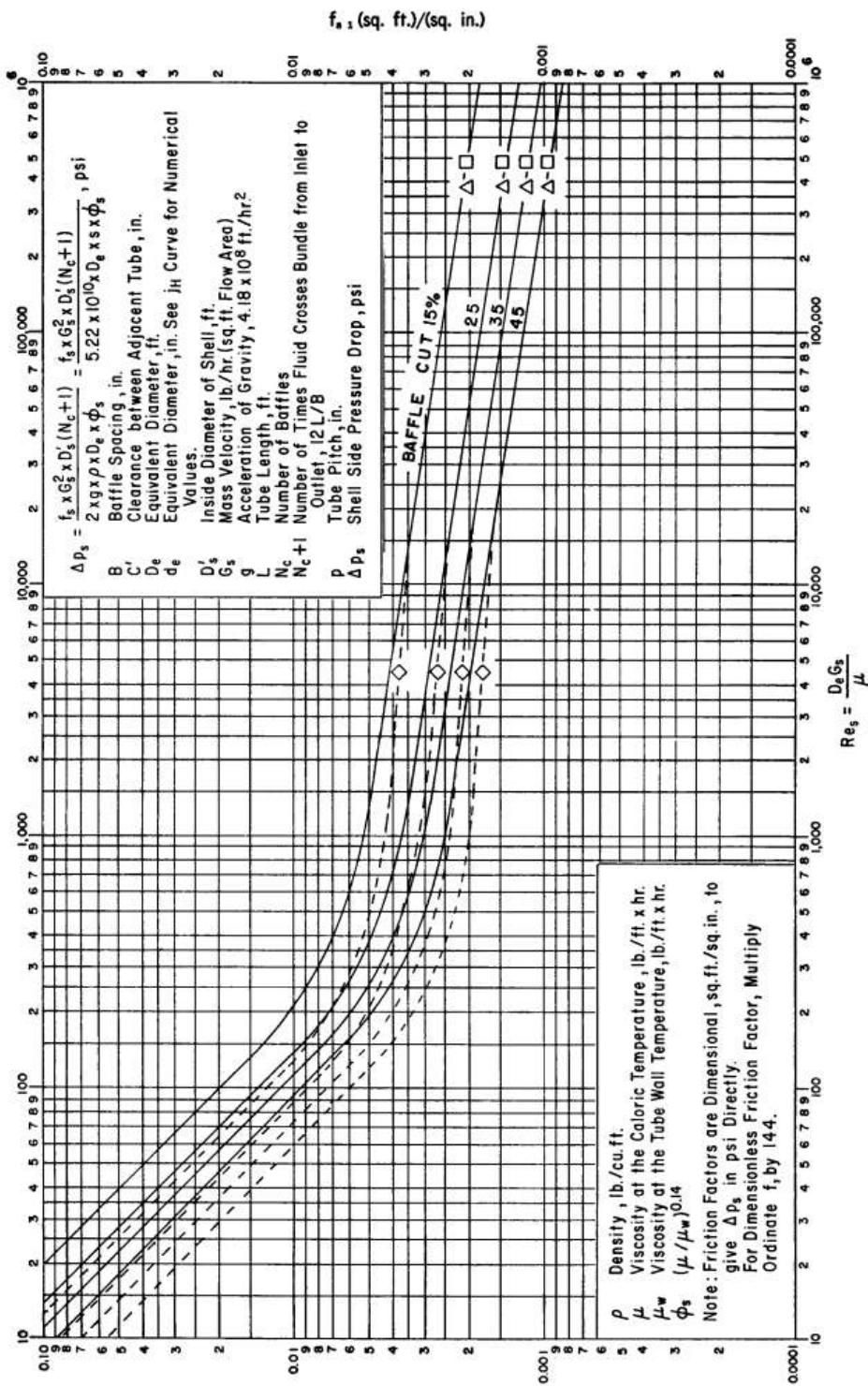


Figure 10-140. Shell-side friction factors for low-finned and plain tubes. (Used by permission: Engineering Data Book, © 1960. Wolverine Tube, Inc.)

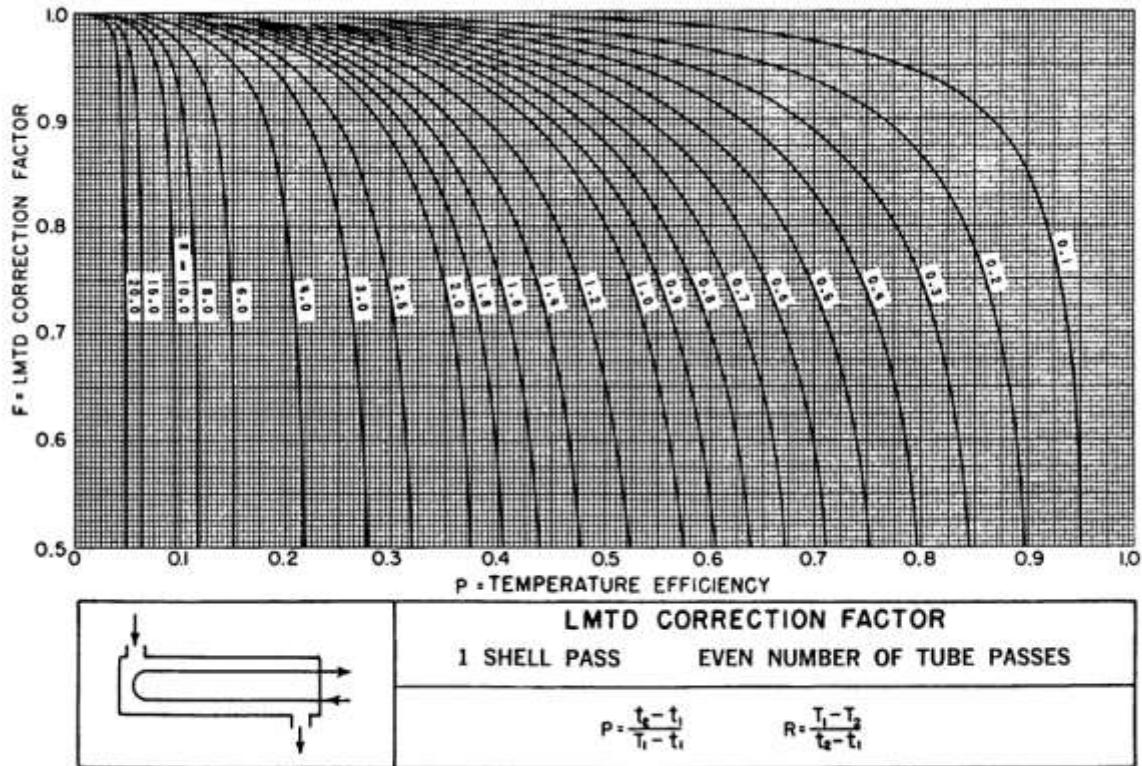


Figure 10-34A. MTD correction factor, 1 shell pass, even number of tube passes. (Figures 10-34A-10-34J used by permission: *Standards of Tubular Exchanger Manufacturers Association*, 7<sup>th</sup> Ed., Figure T-32, ©1988. Tubular Exchanger Manufacturers Association, Inc.)